## Pt. 63, Subpt. UUU, Table 15

[67 FR 17773, Apr. 11, 2002, as amended at 70 FR 6942 and 6948, Feb. 9, 2005]

## Table 15 to Subpart UUU of Part 63—Organic HAP Emission Limits for Catalytic Reforming Units

As stated in  $\S63.1566(a)(1)$ , you shall meet each emission limitation in the following table that applies to you.

For each applicable process vent for a new or existing catalytic reforming unit	You shall meet this emission limit during initial catalyst depressuring and catalyst purging operations
1. Option 1	Vent emissions to a flare that meets the requirements for control devices in §63.11(b). Visible emissions from a flare must not exceed a total of 5 minutes during any 2-hour operating period.
2. Option 2	Reduce uncontrolled emissions of total organic compounds (TOC) or nonmethane TOC from your process vent by 98 percent by weight using a control device or to a concentration of 20 ppmv (dry basis as hexane), corrected to 3 percent oxygen, whichever is less stringent. If you vent emissions to a boiler or process heater to comply with the percent reduction or concentration emission limitation, the vent stream must be introduced into the flame zone, or any other location that will achieve the percent reduction or concentration standard.

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## TABLE 16 TO SUBPART UUU OF PART 63—OPERATING LIMITS FOR ORGANIC HAP EMISSIONS FROM CATALYTIC REFORMING UNITS

As stated in  $\S63.1566(a)(2)$ , you shall meet each operating limit in the following table that applies to you.

For each new or existing catalytic reforming unit	For this type of control device	You shall meet this operating limit during initial catalyst depressuring and purging operations
1. Option 1: vent to flare	Flare that meets the requirements for control devices in § 63.11(b).	The flare pilot light must be present at all times and the flare must be operating at all times that emissions may be vented to it.
Option 2: Percent reduction or concentration limit.	Thermal incinerator, boiler or process heater with a design heat input capacity under 44 MW, or boiler or process heater in which all vent streams are not introduced into the flame zone.	The daily average combustion zone tem- perature must not fall below the limit established during the performance test.
	b. No control device	Operate at all times according to your operation, maintenance, and monitoring plan regarding minimum catalyst purging conditions that must be met prior to allowing uncontrolled purge releases.

 $[67~{\rm FR}~17773,~{\rm Apr.}~11,~2002,~{\rm as~amended~at}~70~{\rm FR}~6942~{\rm and}~6951,~{\rm Feb.}~9,~2005]$ 

## TABLE 17 TO SUBPART UUU OF PART 63—CONTINUOUS MONITORING SYSTEMS FOR ORGANIC HAP EMISSIONS FROM CATALYTIC REFORMING UNITS

As stated in  $\S63.1566(b)(1)$ , you shall meet each requirement in the following table that applies to you.

For each applicable process vent for a new or existing catalytic reforming unit	If you use this type of control device	You shall install and operate this type of continuous monitoring system
1. Option 1: vent to a flare	Flare that meets the requirements for control devices in § 63.11(b).	Monitoring device such as a thermo- couple, an ultraviolet beam sensor, or infrared sensor to continuously detect the presence of a pilot flame.
Option 2: percent reduction or concentration limit.	Thermal incinerator, process heater or boiler with a design heat input capacity under 44 MW, or process heater or boiler in which all vent streams are not introduced into the flame zone.	Continuous parameter monitoring sys- tems to measure and record the com- bustion zone temperature.